

REINHOLD ENVIRONMENTAL Ltd.



**2013 NO<sub>x</sub>-Combustion Round Table  
& Expo Presentations**

February 18 & 19, 2013, in Salt Lake City, UT / Hosted by PacifiCorp

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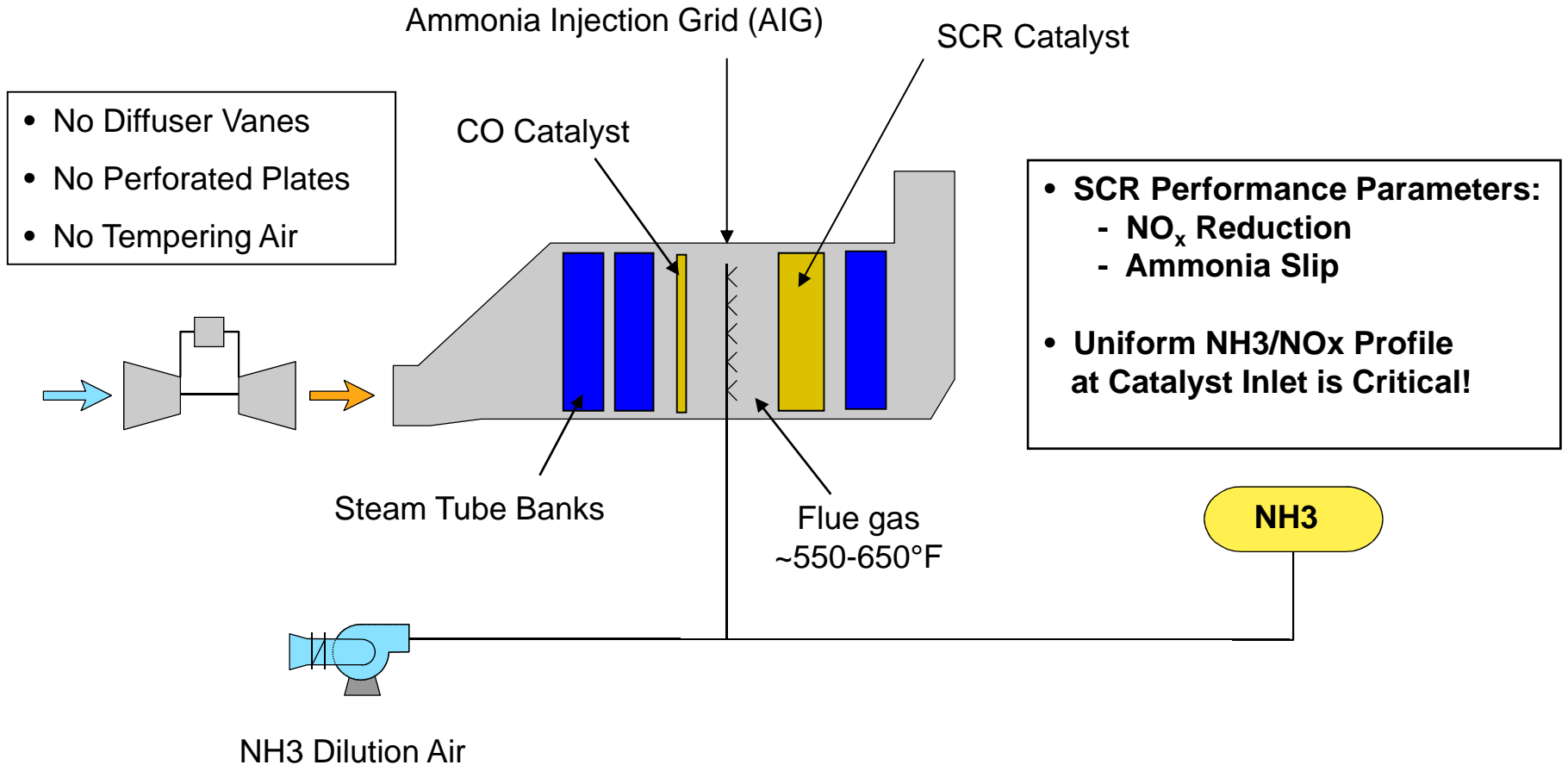
# **Tools for Optimizing Gas Turbine SCR Performance**

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**Laguna Hills, CA**

**Reinhold 2013 NOx-Combustion Round Table**  
**February 18, 2013**  
**Salt Lake City, Utah**



# Cogeneration Gas Turbine SCR

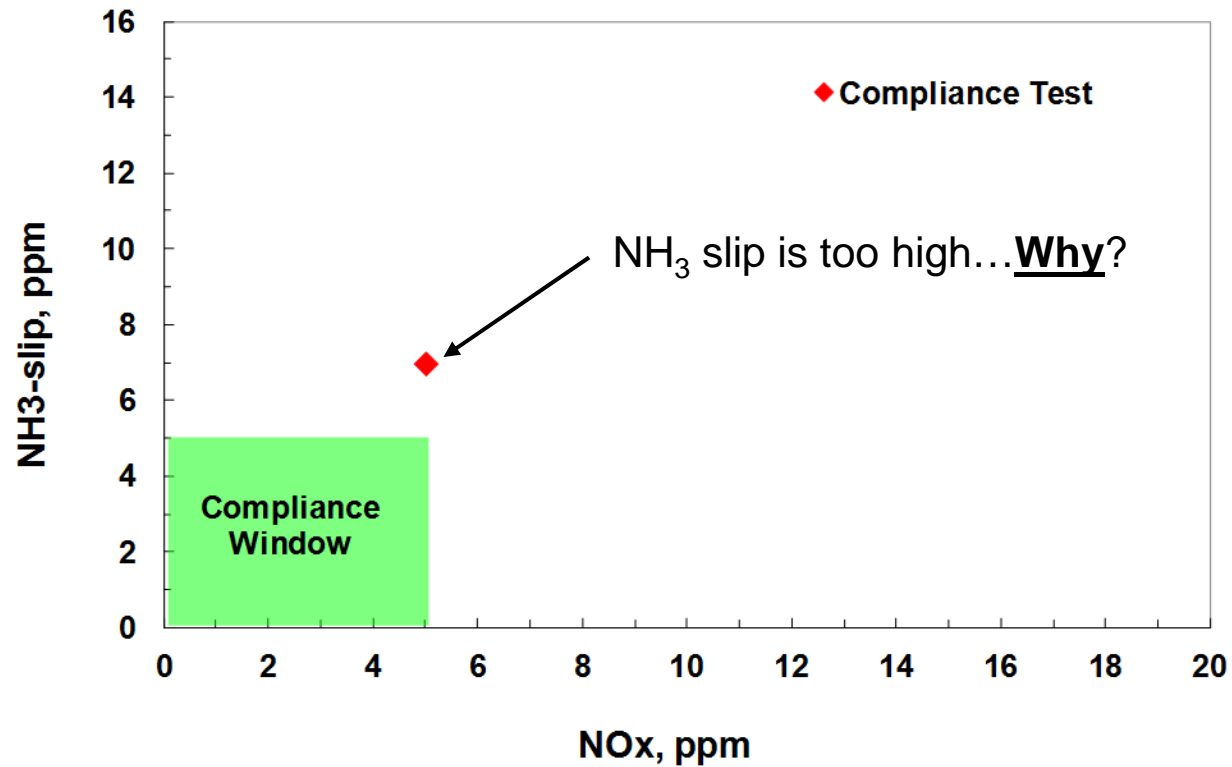


# Optimizing Gas Turbine SCR Performance

## Topics

- **Troubleshooting**
- **Catalyst Inlet NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning**
- **Identifying Flue Gas Bypass (e.g., Leaky Catalyst Seals)**
- **Measuring Catalyst Velocity Distribution**
- **SCR Impact on CEMs Relative Accuracy**
- **Catalyst Management/Measuring Catalyst Activity**

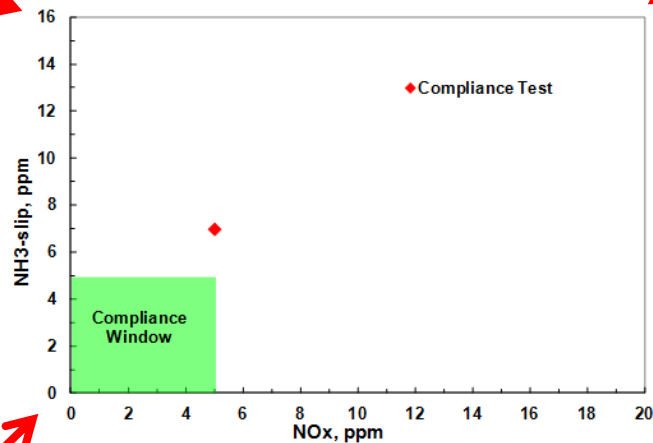
# Troubleshooting



# Why?

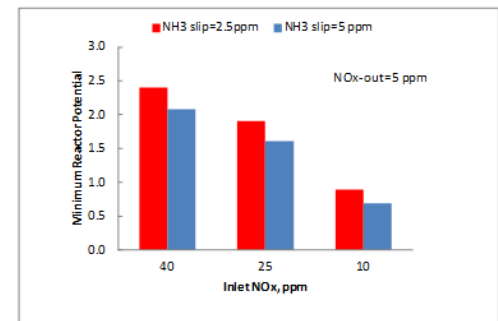
## Catalyst Activity (K)?

- How active the material is in reducing NO<sub>x</sub>
- f(material, geometry)



## Reactor Potential?

- Ability of the catalyst bed to reduce NO<sub>x</sub>
- $RP = K * A_{sp} * V_{cat} / Q_{fg}$



## Poor NH<sub>3</sub>/NO<sub>x</sub> Distribution?

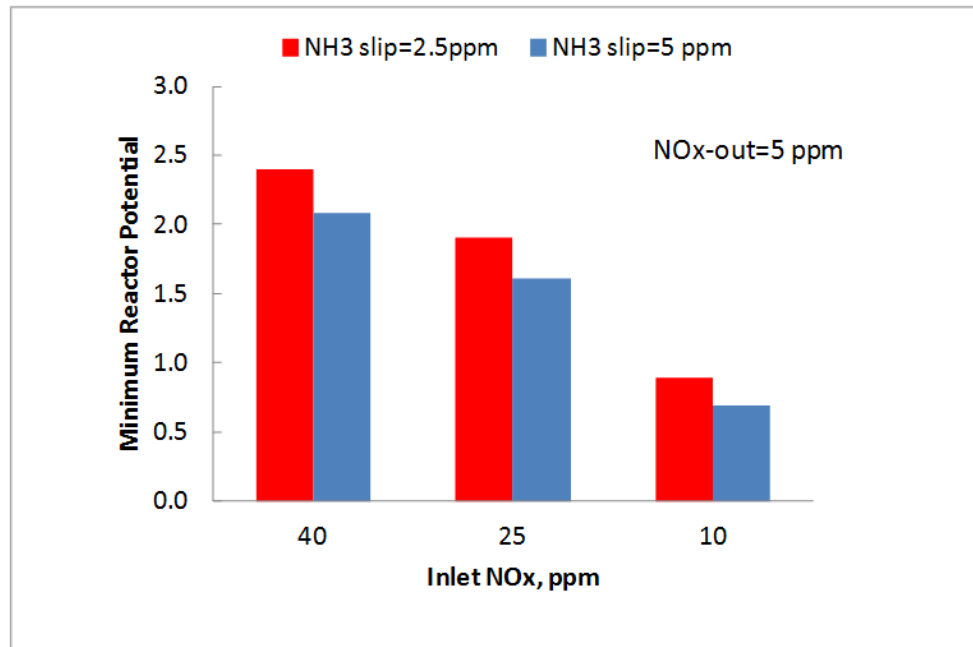
- Want NH<sub>3</sub>/NO<sub>x</sub> uniform across the catalyst
- Local NH<sub>3</sub>/NO<sub>x</sub> > 1 = NH<sub>3</sub> slip

## Flue Gas Bypass?

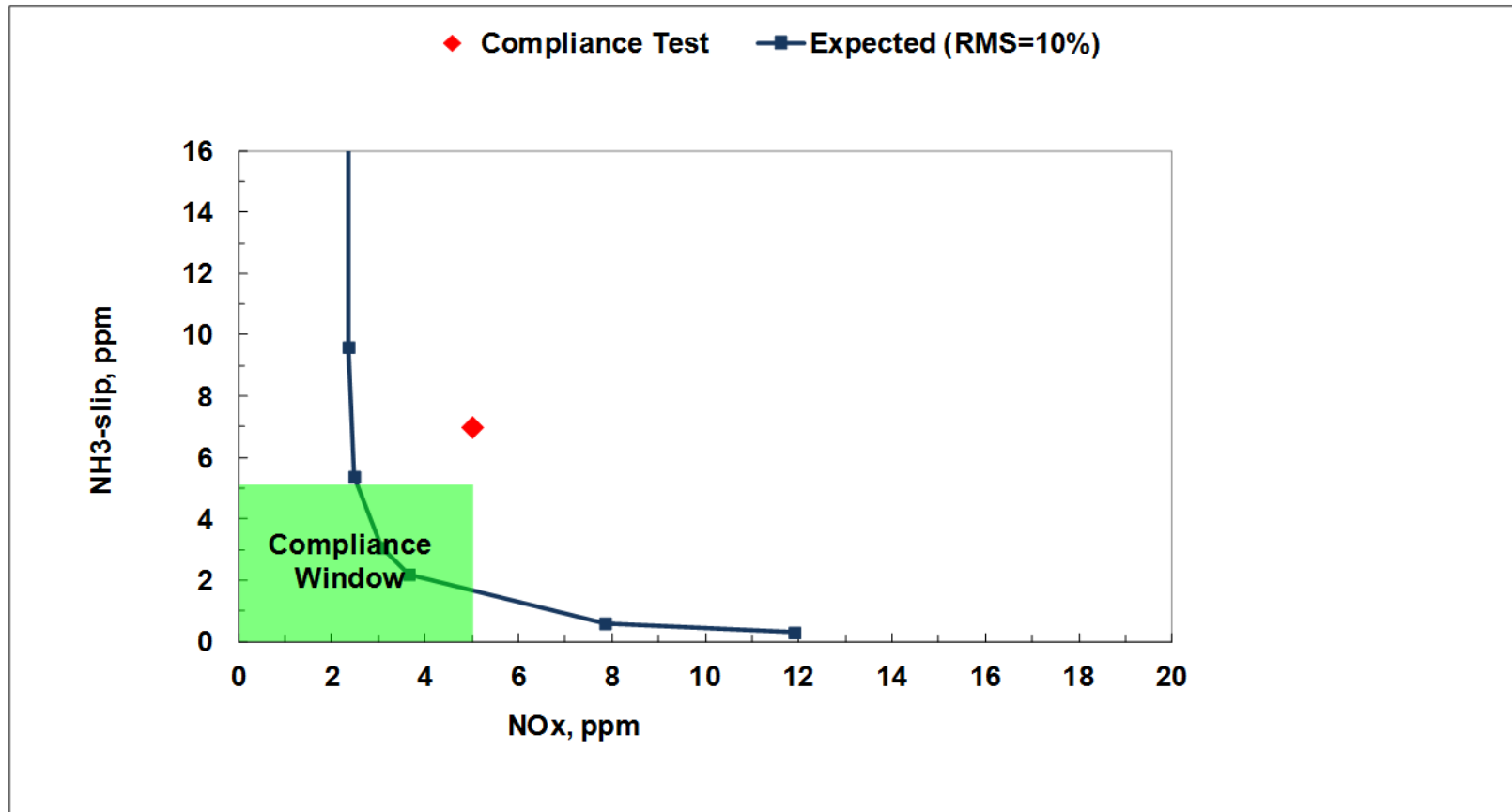
- Any bypass by the catalyst increases stack NO<sub>x</sub> & NH<sub>3</sub>

# Reactor Potential

- Ability of the catalyst bed to reduce  $\text{NO}_x$
- $\text{RP} = K \cdot A_{\text{sp}} \cdot V_{\text{cat}} / Q_{\text{fg}}$
- $\text{RP} = f(\text{NO}_{x,i}, \Delta\text{NO}_x, \text{and } \text{NH}_3 \text{ slip})$



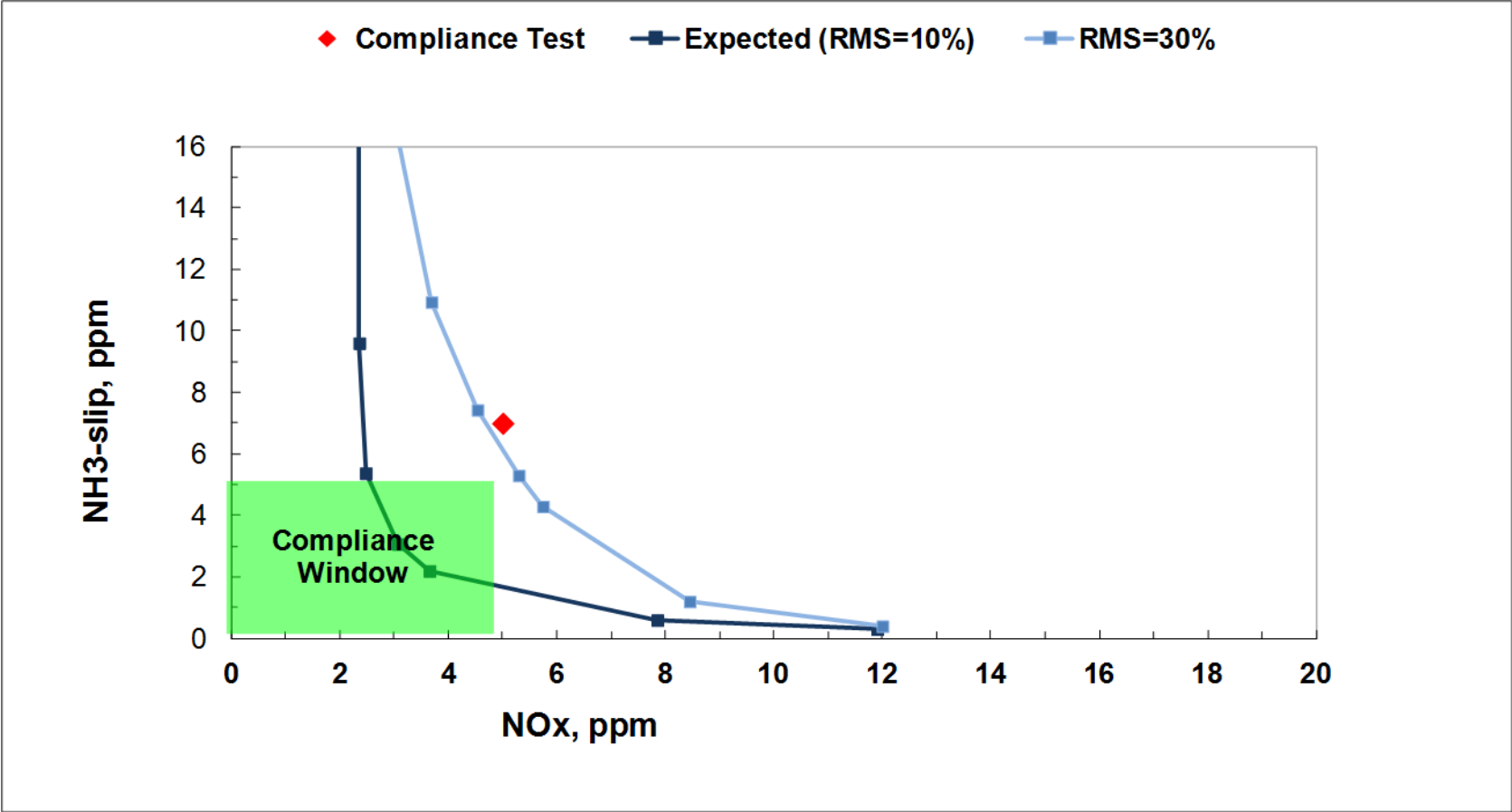
# Expected Performance Based on Catalyst Properties



- Reactor Potential (RP) and is catalyst activity are typically adequate for new or young catalyst

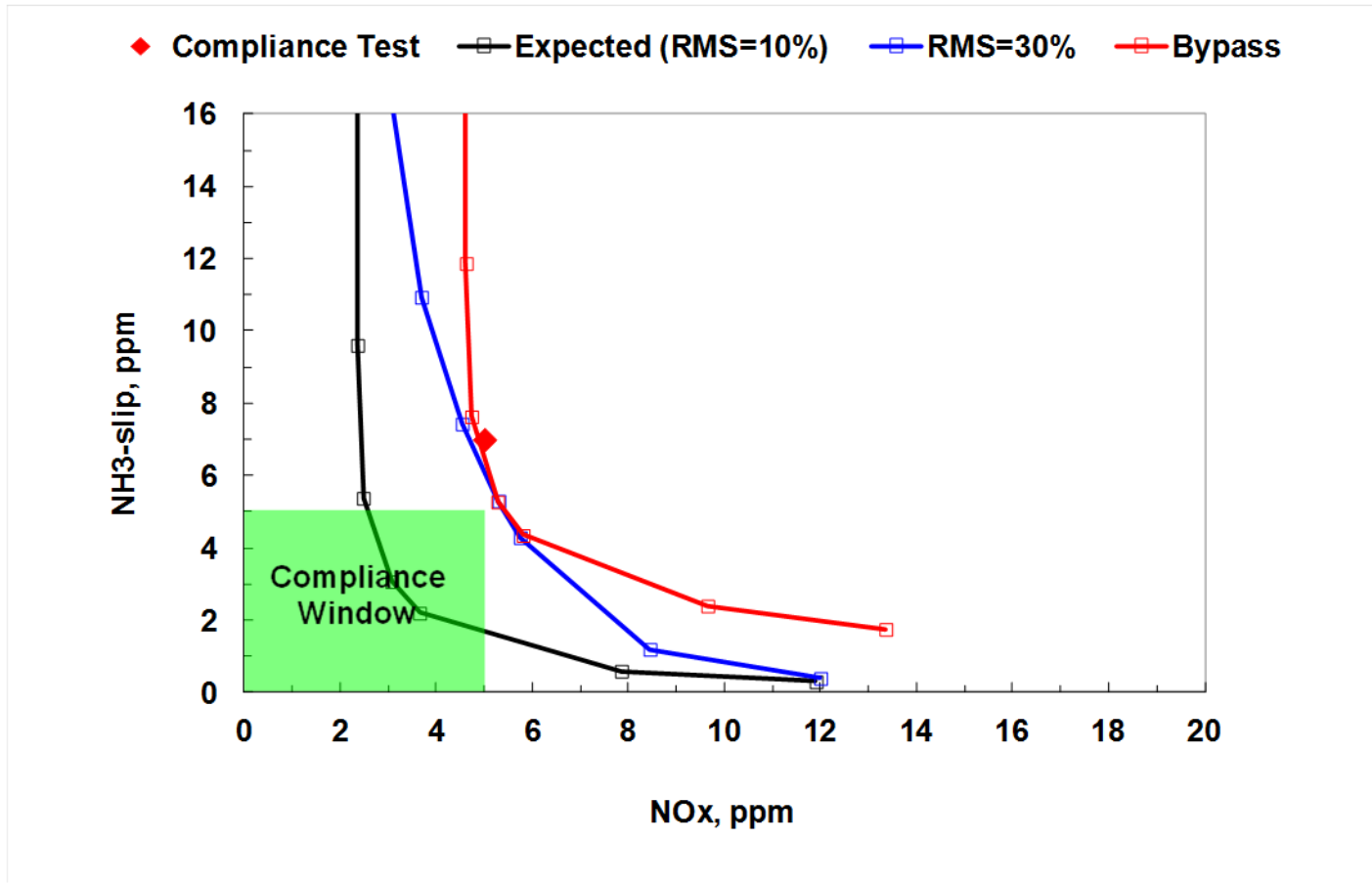
- Exception: unexpected high temperatures

# Poor NH3/NOx Distribution?

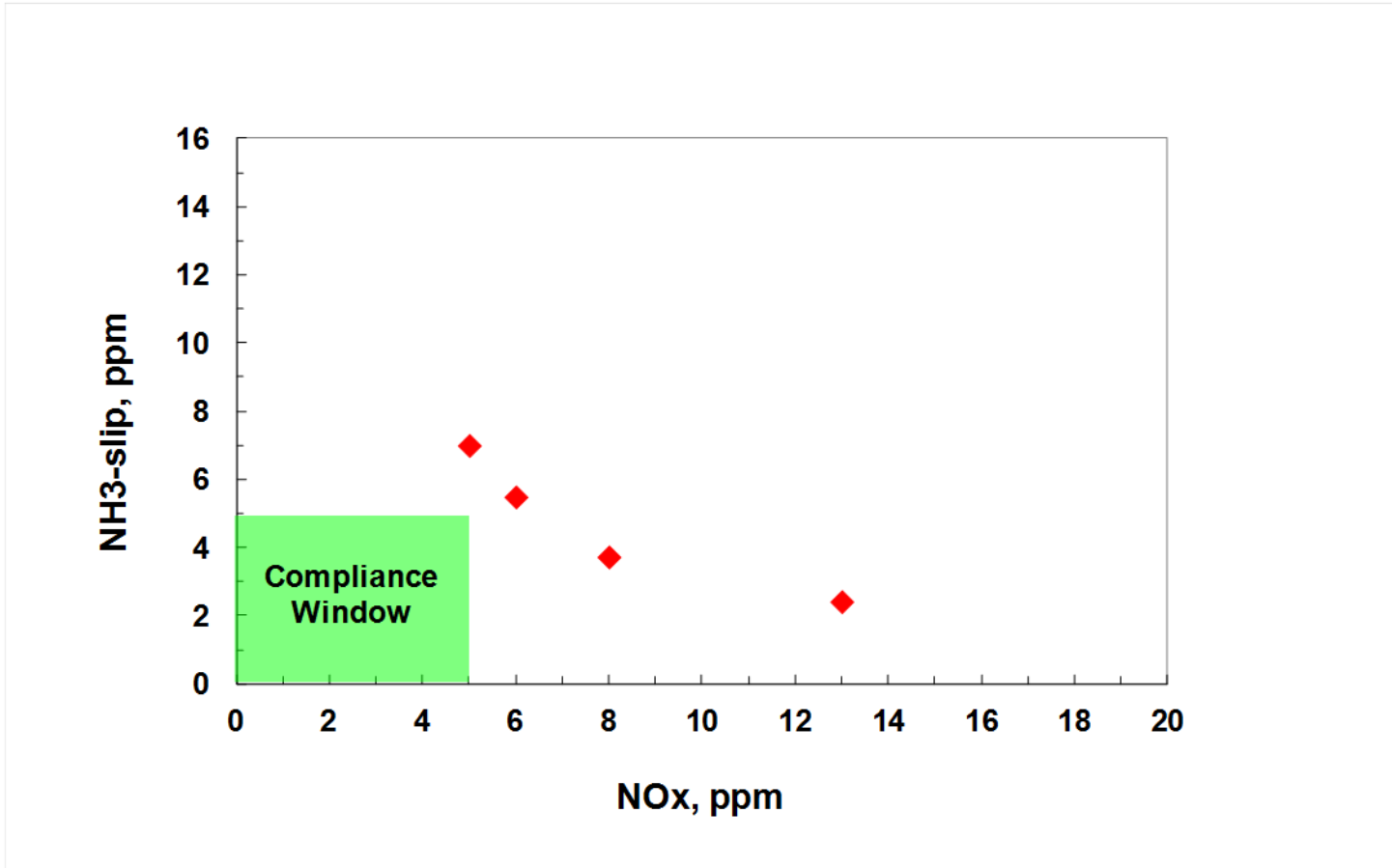


# Flue Gas Bypass?

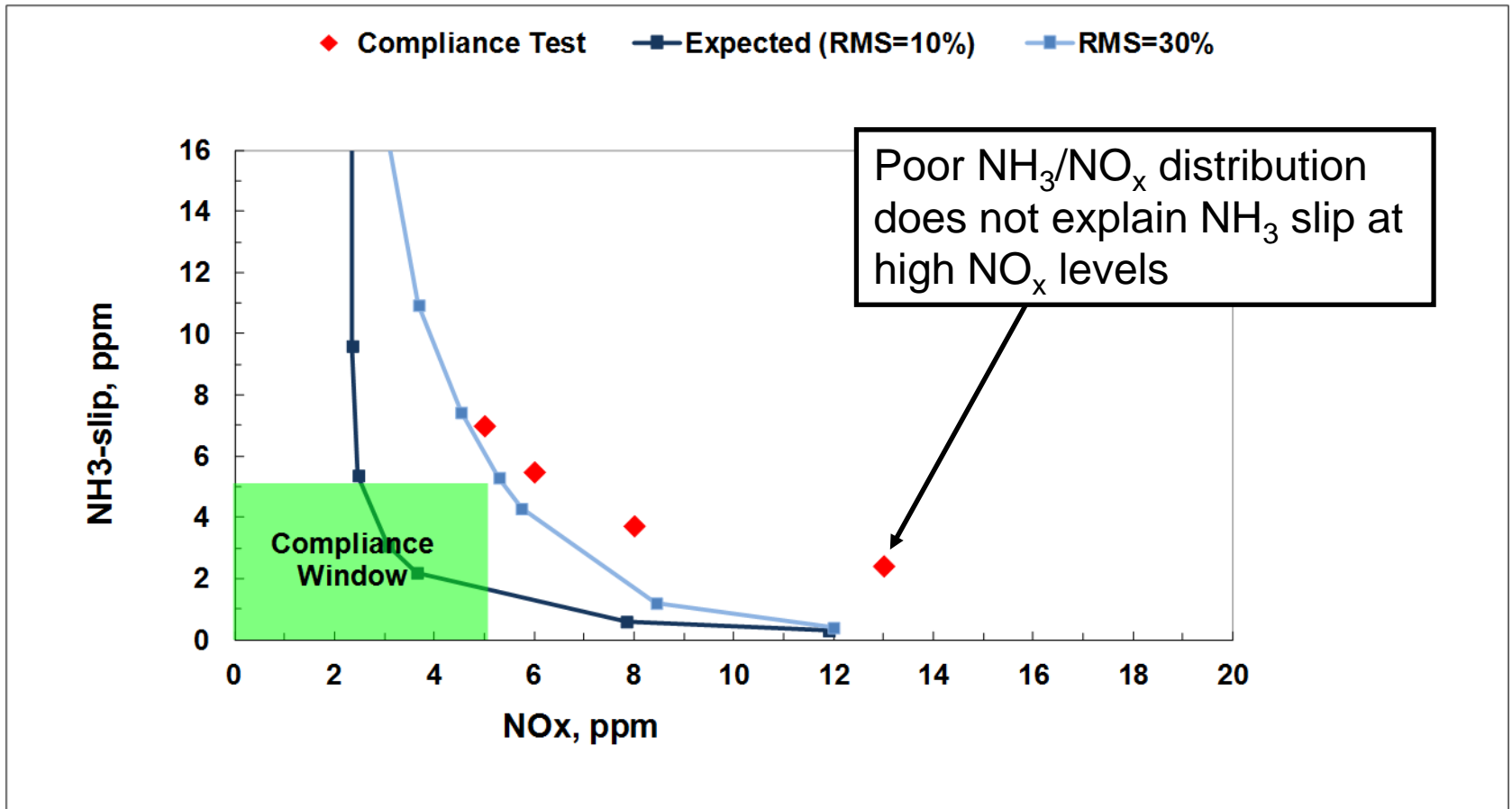
With a single test it is difficult to determine the reason for non-compliance



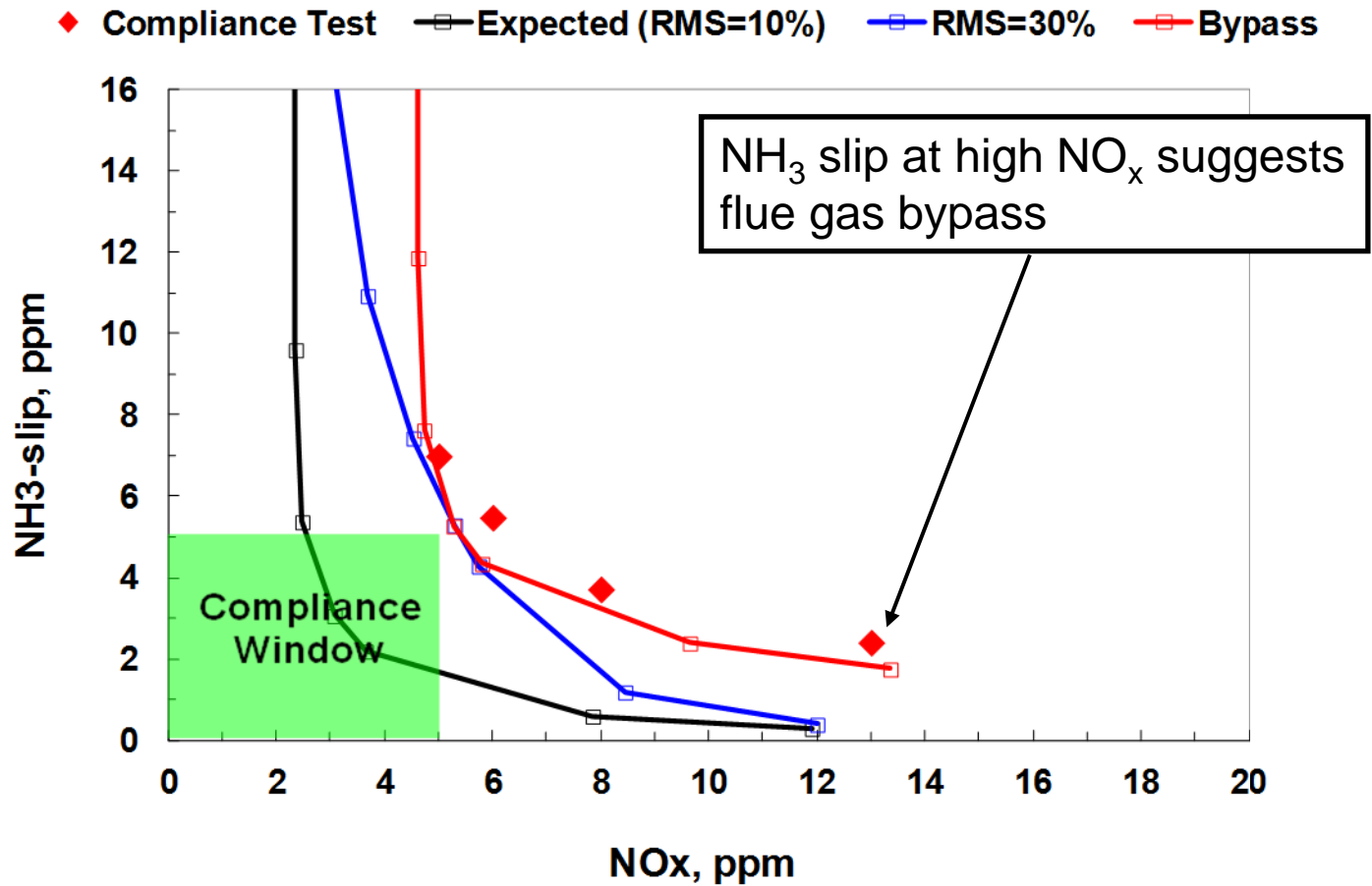
# Perform Additional Tests



# Poor NH<sub>3</sub>/NO<sub>x</sub> Distribution?



# Flue Gas Bypass?

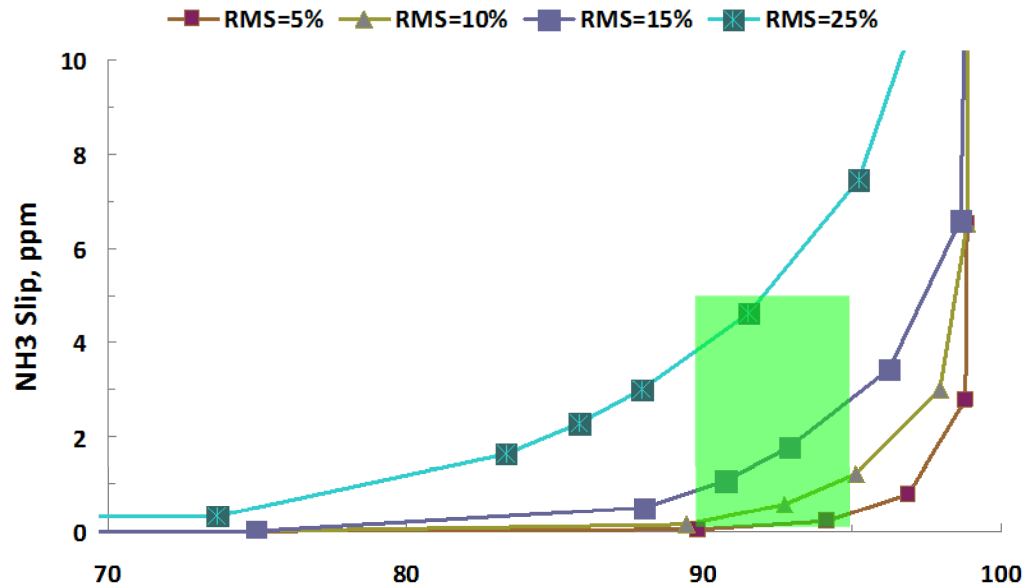


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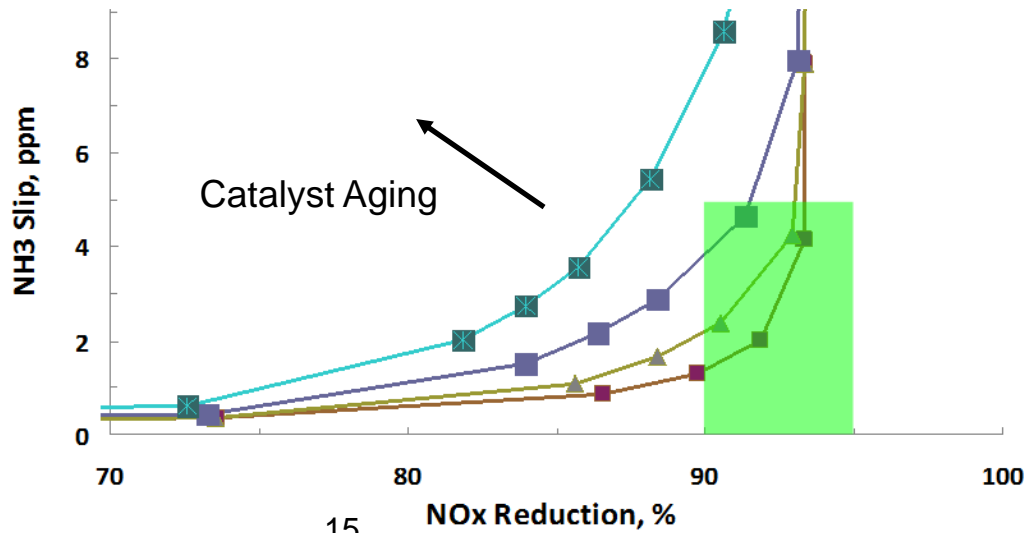
# Catalyst Inlet NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning

# NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning

New Catalyst



Near Catalyst End-of-Life



# Sample Probe Grid Expedites Tuning



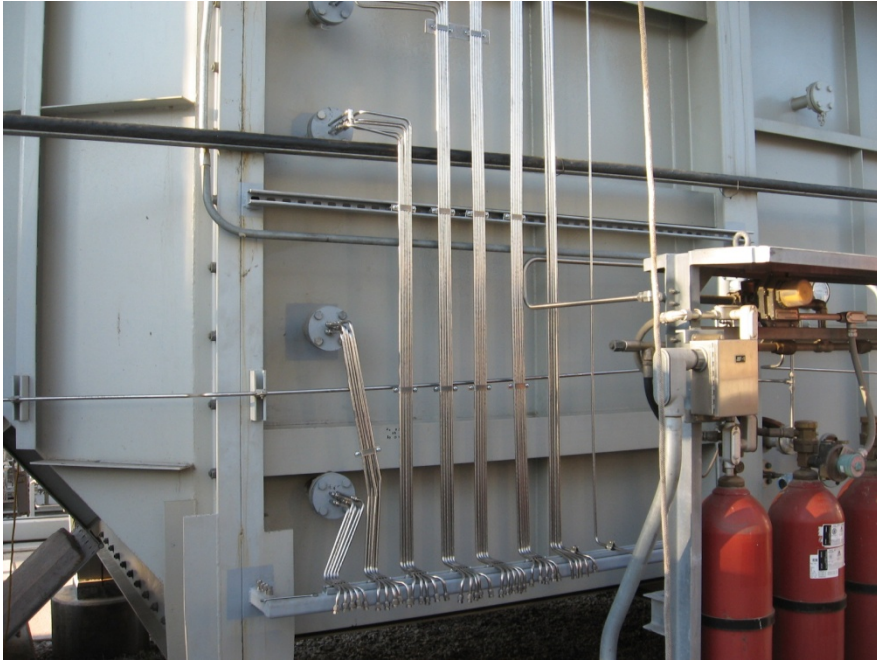
- AIG tuning is difficult without a probe grid at the catalyst exit
- The costs for installing a probe grid will be recovered in the long run:
  - No scaffolding or manlift required for testing (\$, safety issues)
  - Reduced test times (no manual probe)
  - Reduced testing contractor costs
  - More data

**50MW simple cycle SCR  
With a grid of 50 sample probes  
(5 x 10)**

# Sample Probe Grid Expedites Tuning



# Sample Probe Grid Expedites Tuning



# Sample Probe Grid Expedites Tuning



# FERCo's Multipoint Instrumentation

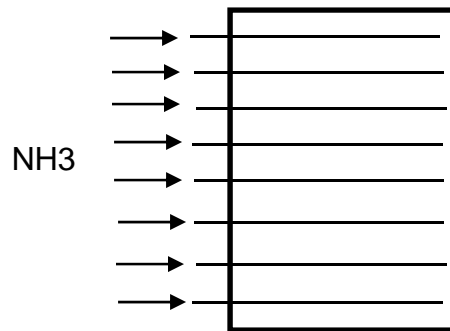


- Samples 48 points in 15 minutes
- NO<sub>x</sub> and O<sub>2</sub>



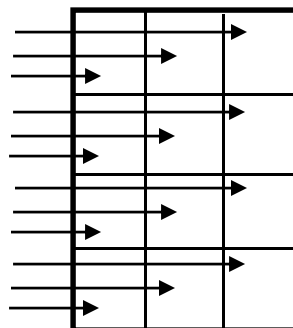
# AIG Design Influences Tuning

- **No Adjustments:** Some systems have no AIG adjustment valves – *bad idea!* No flexibility to account for 1) duct velocity gradients, 2) duct NOx gradients, or 3) lance-to-lance ammonia flow gradients
- **1-D:** Most systems have one-dimensional adjustability



Vertical adjustability can handle only vertical gradients

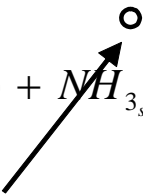
- **Multi-Zone:** Ideal design: multiple zone adjustability



Multiple zones allow treatment of localized gradients

# AIG Tuning Procedure

**Basis** (SCR operated with no local NH<sub>3</sub> slip)

$$NH_{3\text{in}_i} = (NO_{x\text{in}_i} - NO_{x\text{out}_i}) + NH_{3\text{slip}_i}$$


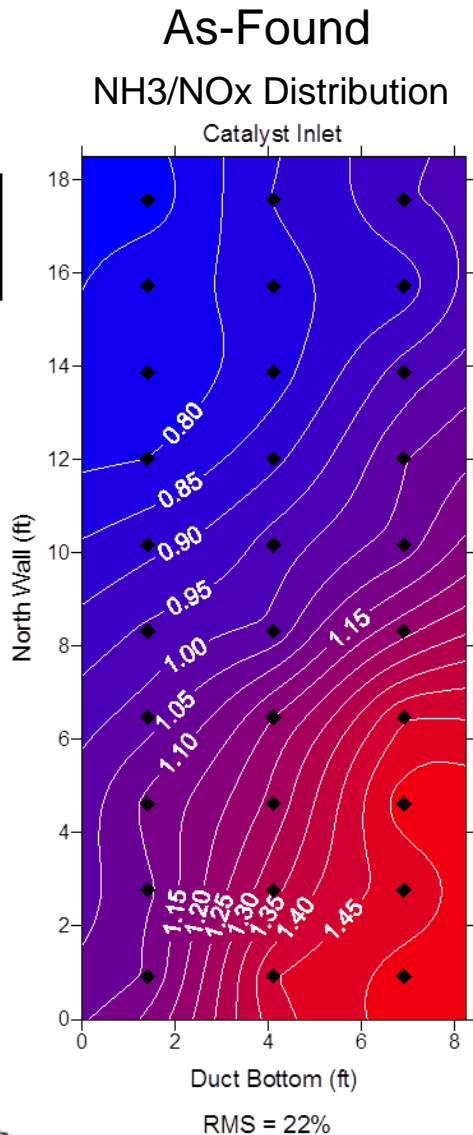
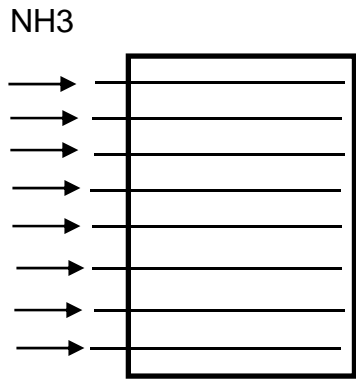
$$\left( \frac{NH_3}{NO_x} \right)_i = \left( 1 - \frac{NO_{x\text{out}_i}}{NO_{x\text{in}_i}} \right)$$

## **Procedure**

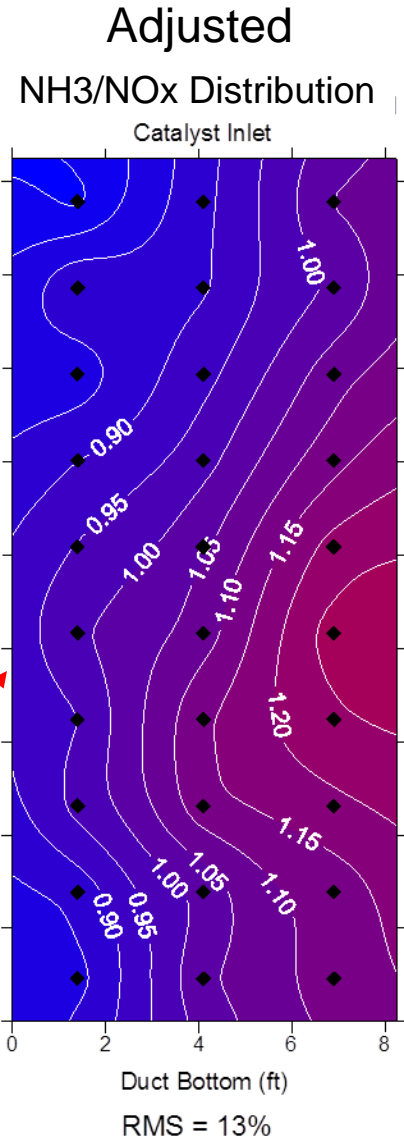
1. Turn off NH<sub>3</sub>, obtain NO<sub>x</sub> outlet profile
2. Turn NH<sub>3</sub> on to produce 50-70% ΔNO<sub>x</sub>, obtain NO<sub>x</sub> outlet profile
3. Use 1 and 2 to calculate local NH<sub>3</sub>/ NO<sub>x</sub> ratios
4. Make contour plot of NH<sub>3</sub>/ NO<sub>x</sub> distribution
5. Adjust AIG and repeat 2-4

# AIG Tuning, 10 MW Gas Turbine SCR

One-Dimensional,  
Vertical AIG

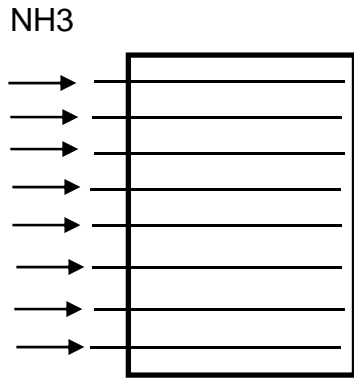


Adjustments  
across the width  
not possible

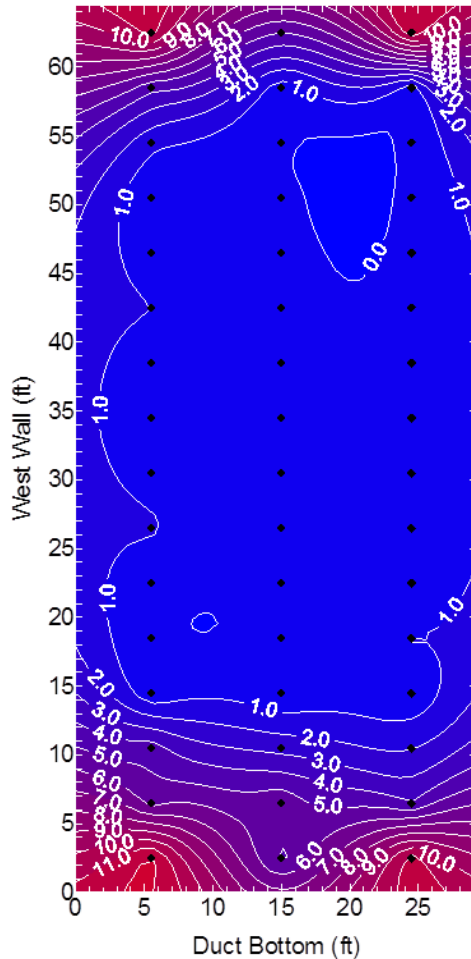


# AIG Tuning, 350MW Combined Cycle SCR

One-Dimensional,  
Vertical AIG

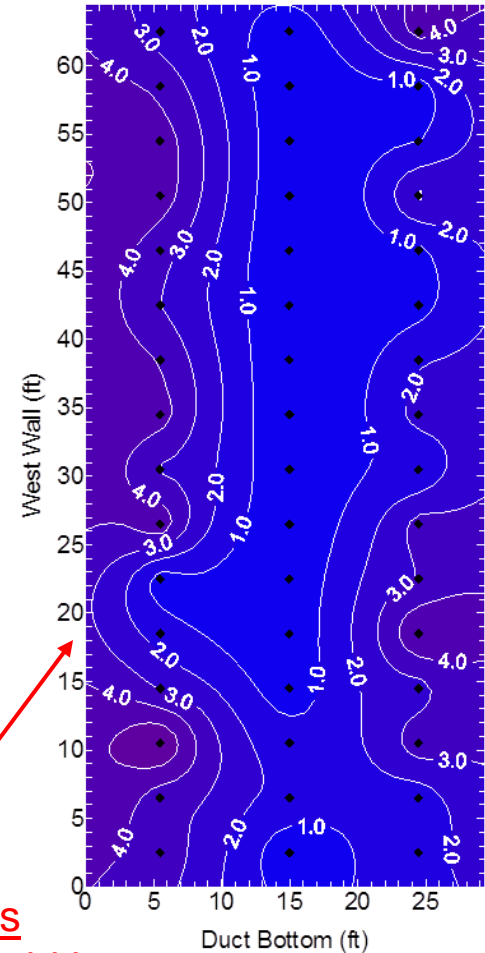


As-Found Outlet  
NOx (ppm)



**NH<sub>3</sub> consumption  
reduced by 5%**

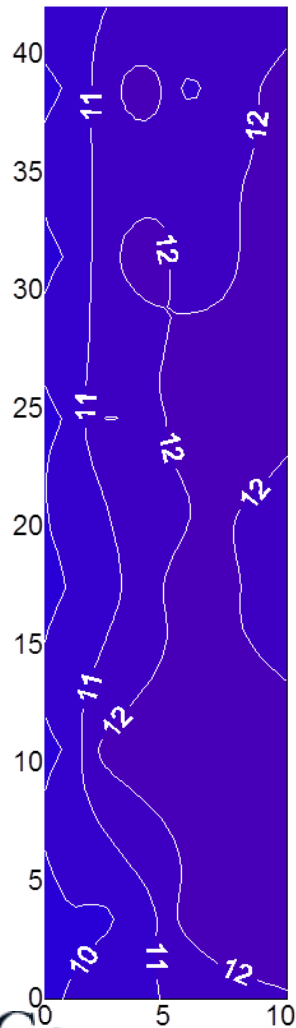
Optimized Outlet  
NOx (ppm)



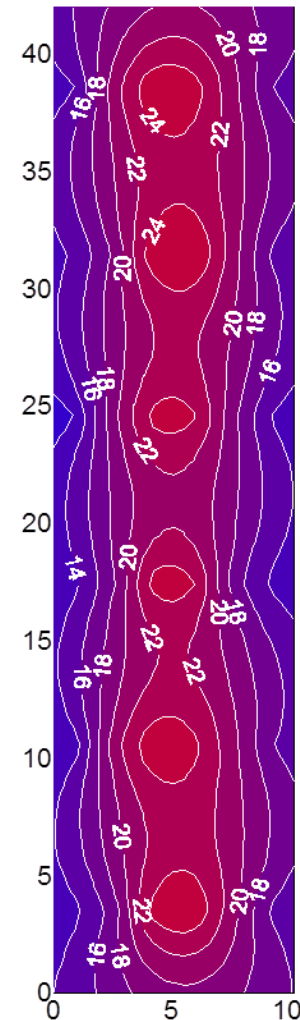
Adjustments  
across the width  
not possible

# Duct Burners Impact AIG Tuning

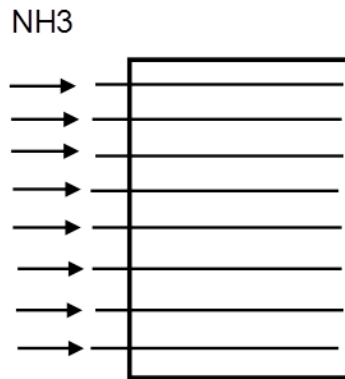
Duct Burners Off  
(Inlet NO<sub>x</sub> ppm)



Duct Burners On  
(Inlet NO<sub>x</sub> ppm)



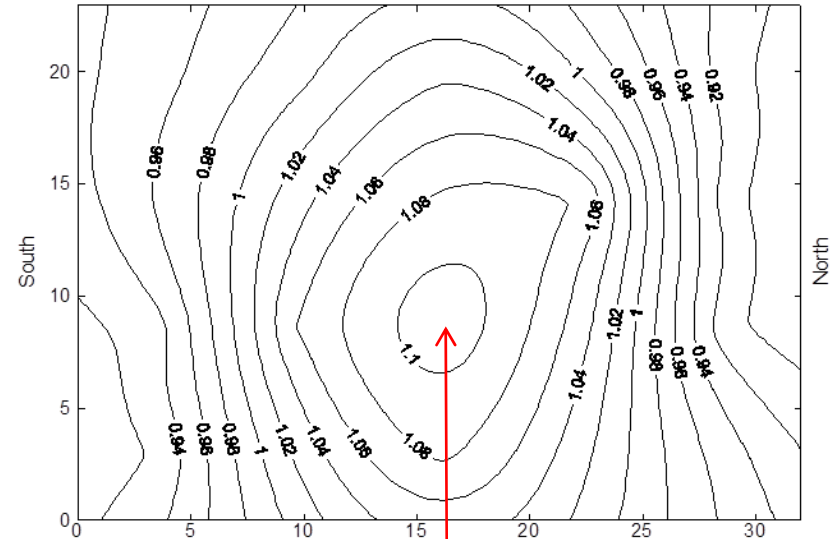
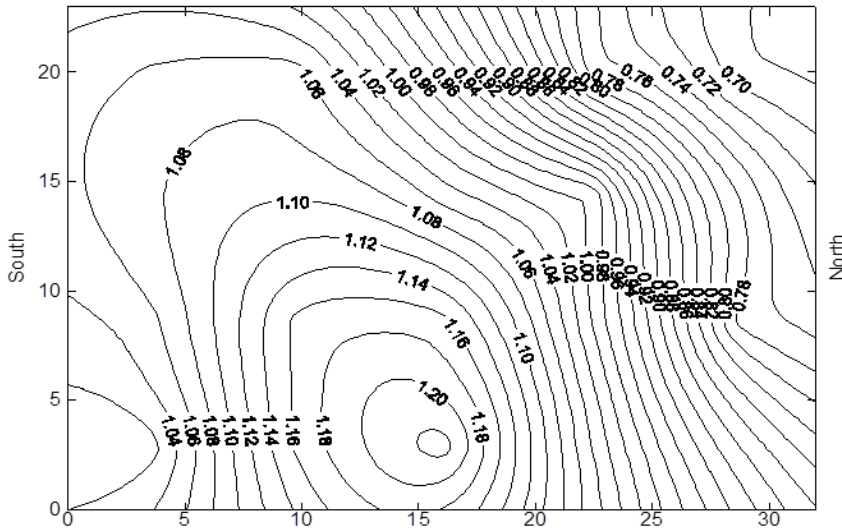
**AIG Tough to Tune**



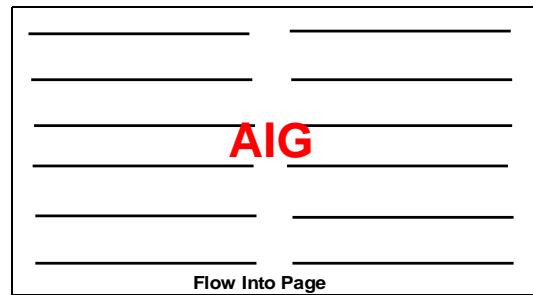
# AIG Tuning, 14 MW Gas Turbine SCR

**As-found (RMS = 14.7%)**

**Optimized (RMS = 6.5%)**

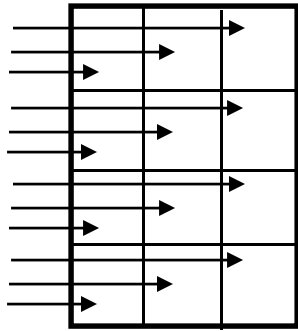


Vertical AIG,  
Two Horizontal Zones

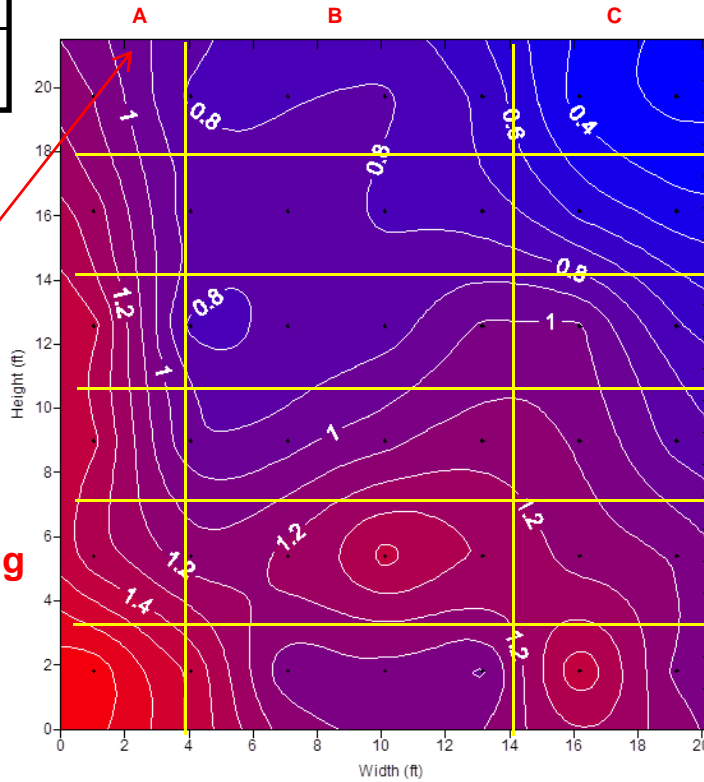


No way to adjust  
the center

# AIG Tuning, 10 MW Gas Turbine SCR, 90° Turn



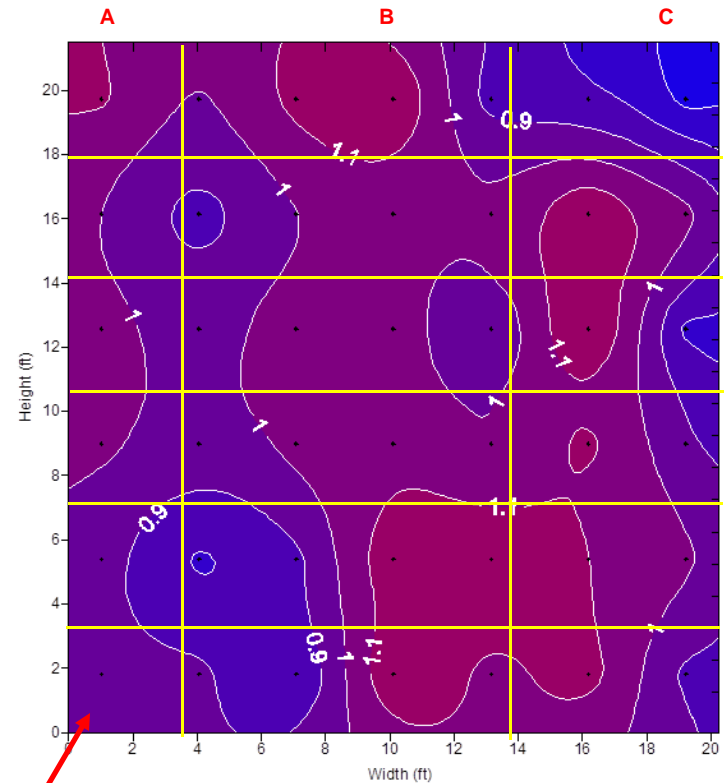
**As-Found**  
Normalized NH<sub>3</sub>/NO<sub>x</sub> Distribution



Multiple zones,  
skewed based  
on flow modeling

RMS = 32%

**Tuned**  
Normalized NH<sub>3</sub>/NO<sub>x</sub> Distribution



Corners adjusted

RMS = 13%

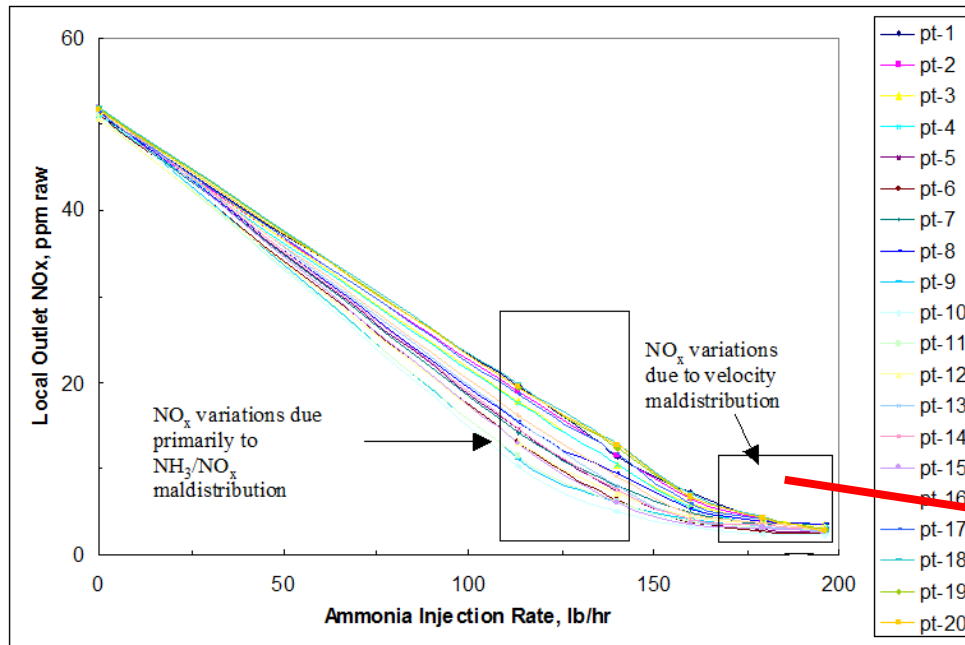
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# Measuring Catalyst Velocity Distribution

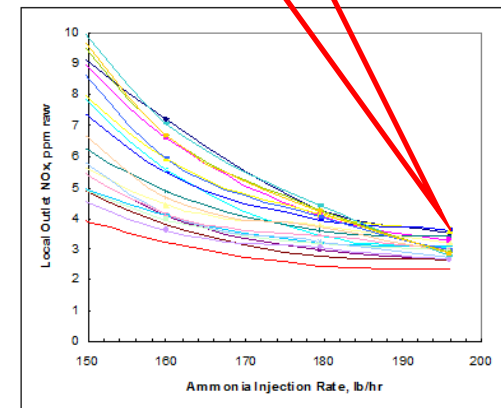
# Catalyst Velocity Distribution

- **Velocity uniformity typically in the specification**
- **Velocity uniformity established during the SCR Design (Cold Flow and/or CFD)**
- **Can it be measured at full scale?**
  - Difficult; large reactors, long probes, low velocities (~15 ft/sec)
  - Pitot Probes, Thermal Anemometers
  - Pitot Probe dPs ~0.02 in H<sub>2</sub>O
  - Velocity profile re-aligns very close to the surface
- **Velocity distribution can be inferred using NO<sub>x</sub> measurements**

# Local Outlet NO<sub>x</sub> VS. NH<sub>3</sub> Injection Rate



$$dNO_x = 1 - e^{-K/Av}$$



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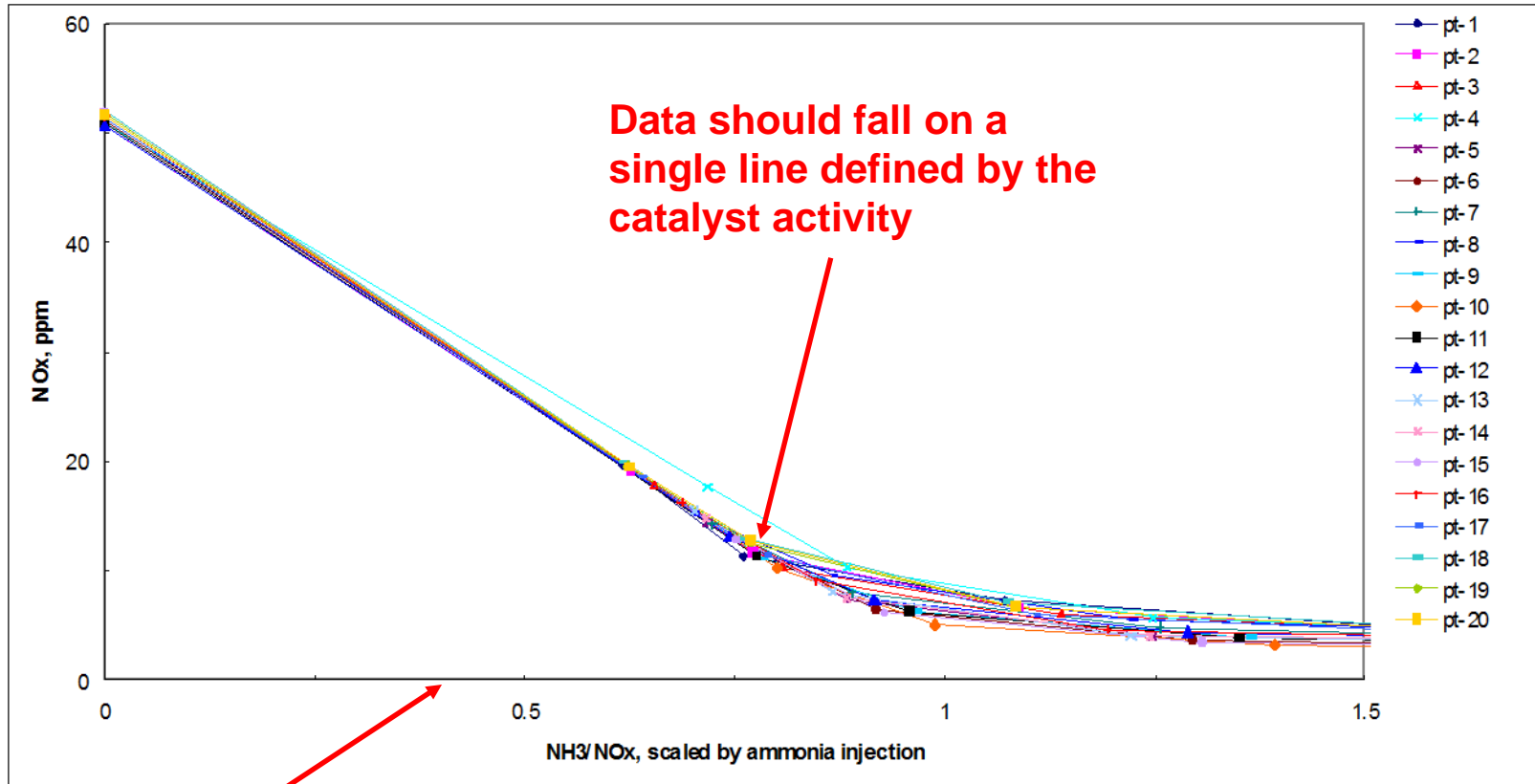
# Identifying Flue Gas Bypass

# Flue Gas Bypass

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- **Improper perimeter seals**
- **Improper seals between catalyst modules**
- **Difficult to diagnose just looking at overall performance**
- **A likely region of bypass is the roof**

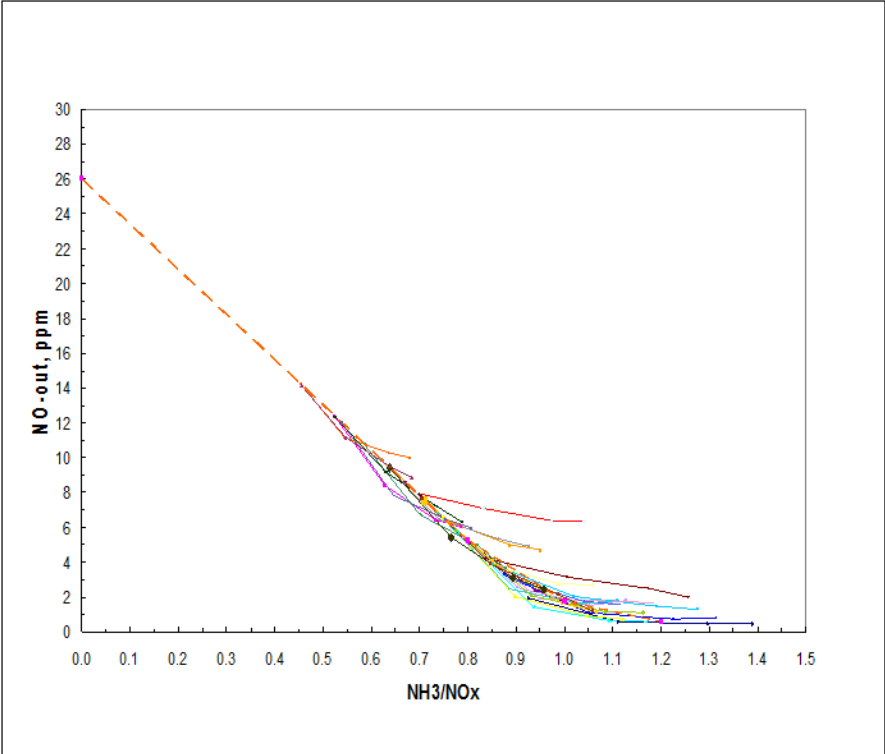
# Flue Gas Bypass



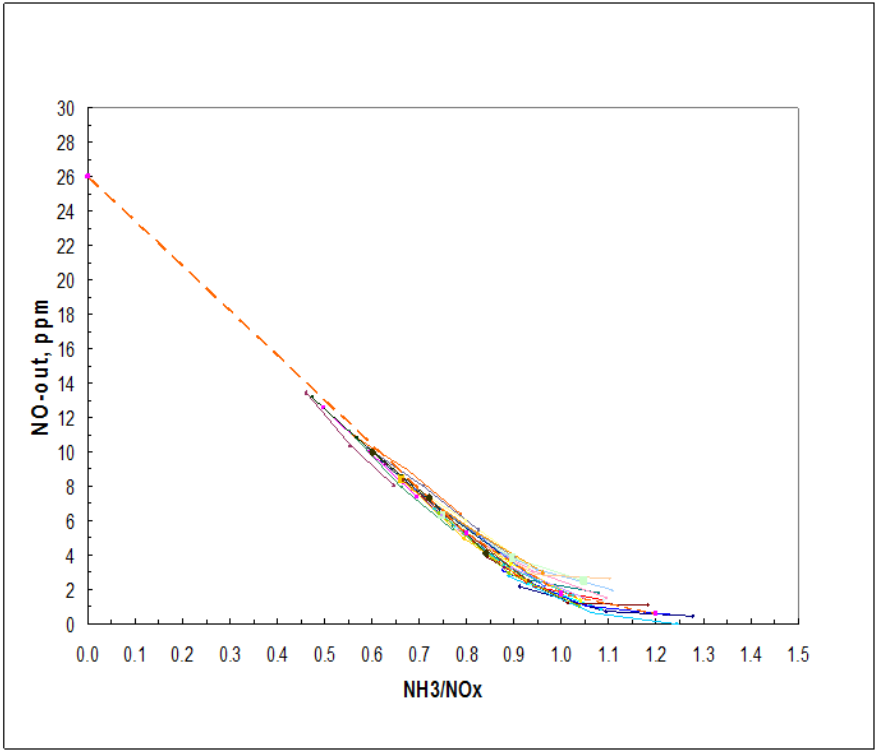
Plot Local NH3/NOx rather than ammonia injection rate

# Flue Gas Bypass, 50 MW Gas Turbine SCR

As-Found



Repaired



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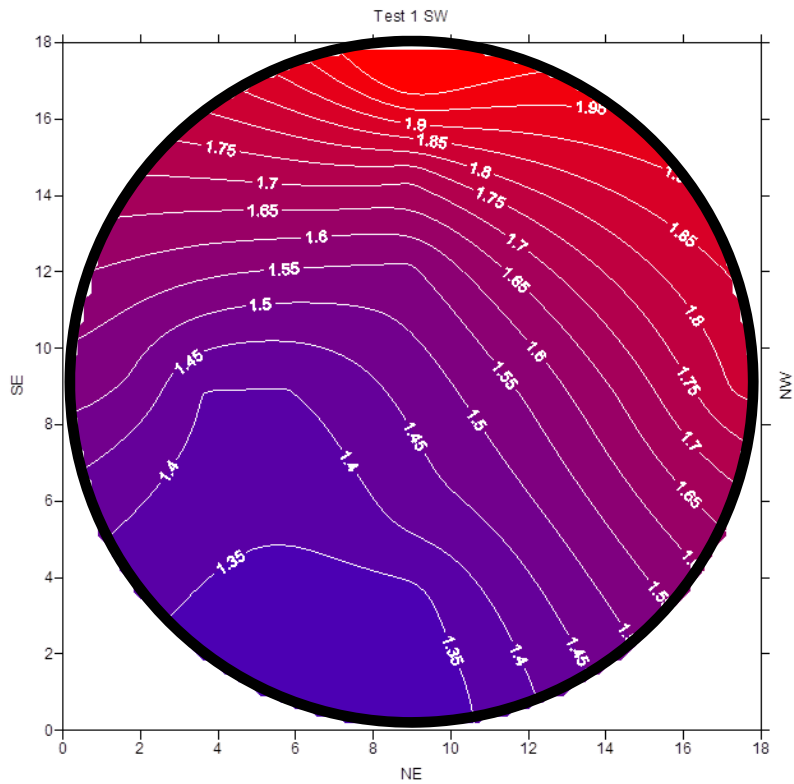
# SCR Impact on CEMs Relative Accuracy

# CEMs Relative Accuracy

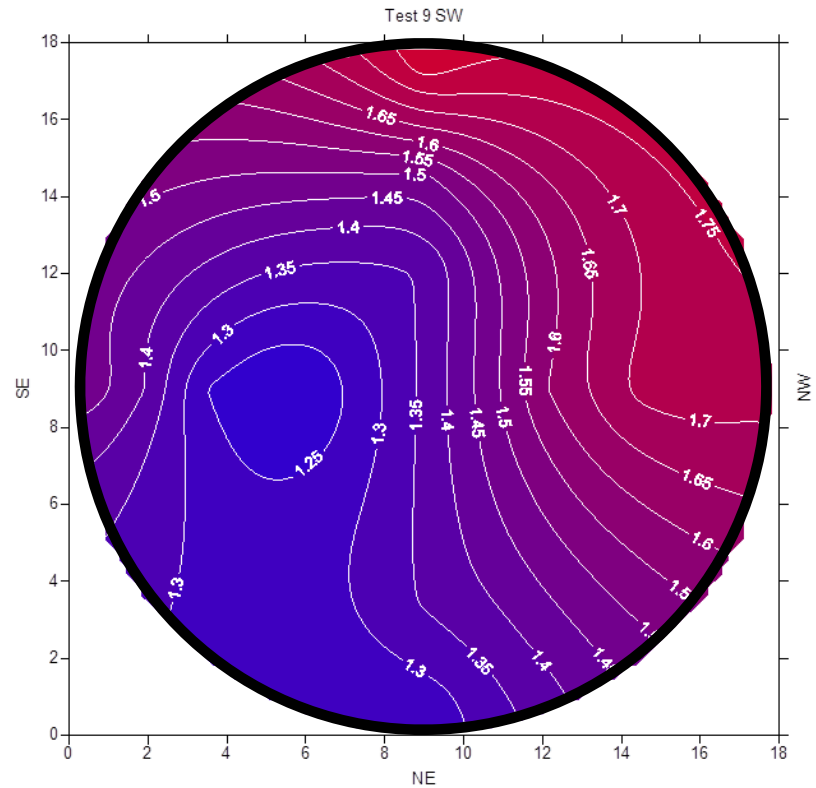
- **NH<sub>3</sub>/NO<sub>x</sub> gradients at the catalyst inlet create NO<sub>x</sub> gradients at the exit of the catalyst**
- **Close proximity of the stack CEMs to the catalyst exit on a gas turbine simple cycle SCR system may result in a stratified NO<sub>x</sub> profile at the CEMs**
- **It may be necessary to tune the AIG specifically to pass the Relative Accuracy Test**

# Relative Accuracy Example

**As Found (RA=-25%)**



**Tuned (RA=-6.6%)**



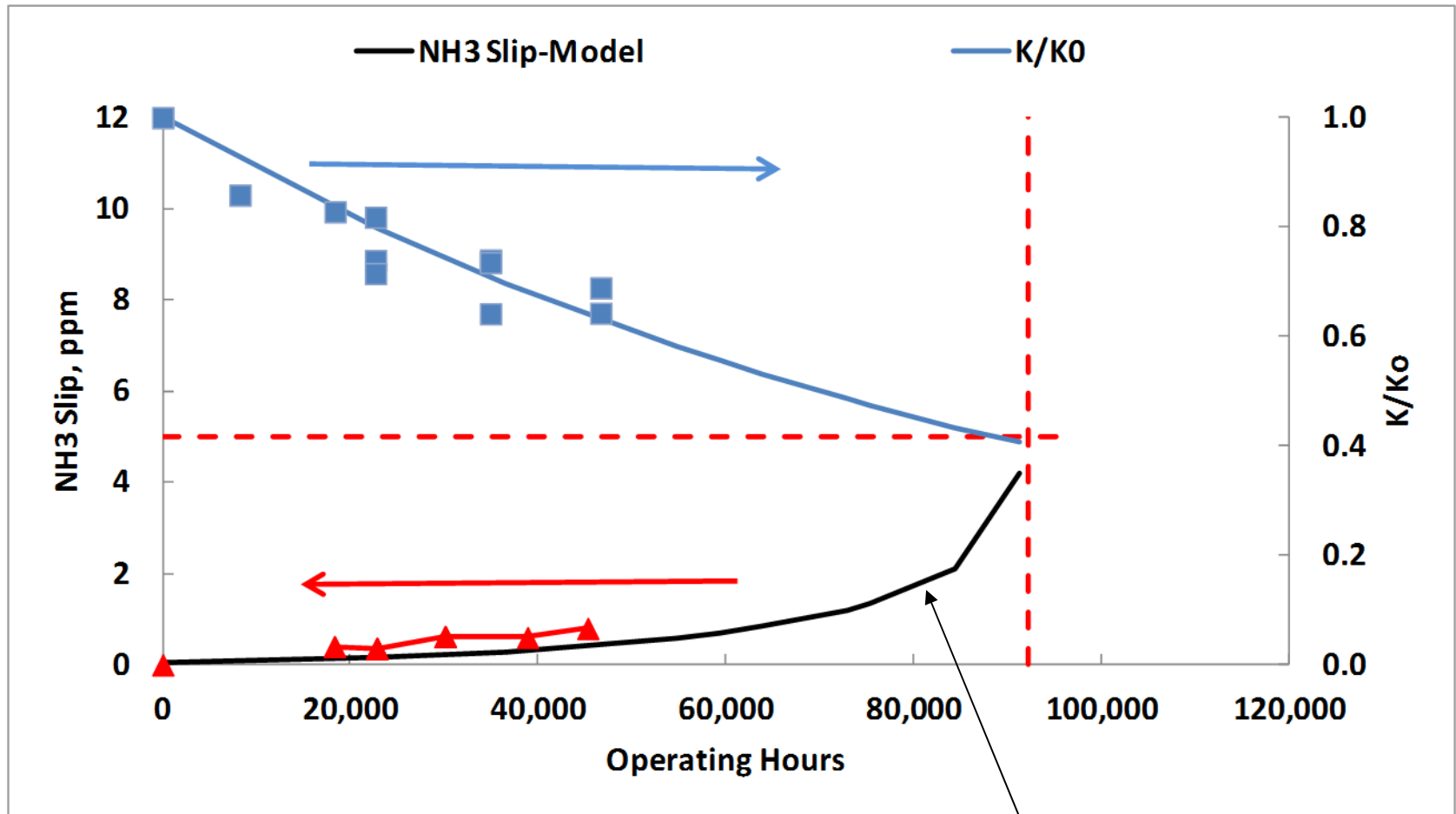
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# Catalyst Management

# Catalyst Management

- **What is Catalyst management?**
  - Keeping track of catalyst activity to ensure continued compliance
- **How is Catalyst Management Done?**
  - Periodically determining the activity of the catalyst in the reactor
  - Laboratory analysis (if a sample can be obtained)
  - In situ analysis (later discussion topic)
  - Utilize catalyst management software for planning
- **Why is it Done?**
  - Forecast when catalyst additions or replacements are necessary
  - Provide sufficient lead time to procure catalyst (6-9 months)

# Catalyst Activity Degrades With Time



Monitoring ammonia slip is also critical

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# In Situ Catalyst Activity Measurements

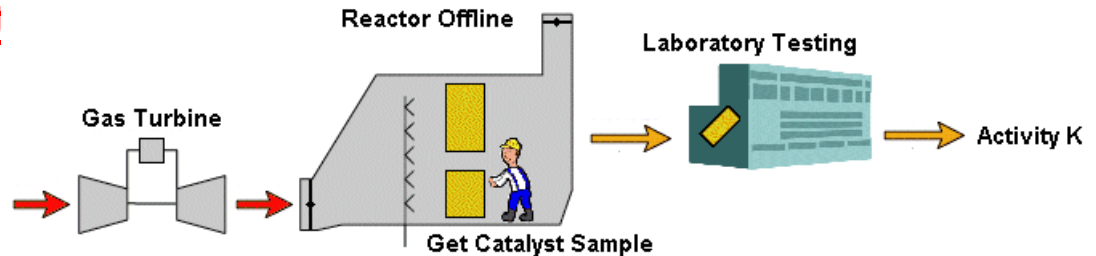
# *In Situ* Catalyst Activity Measurement\*

## Traditional Lab Measurement

- Typically one per year
- Currently no test protocol

$$K_{\text{Lab}} = -A_{\text{Vdesign}} \ln(1 - \Delta\text{NO}_x)_{\text{Lab}}$$

@NH<sub>3</sub>/NO<sub>x</sub>=1-1.5

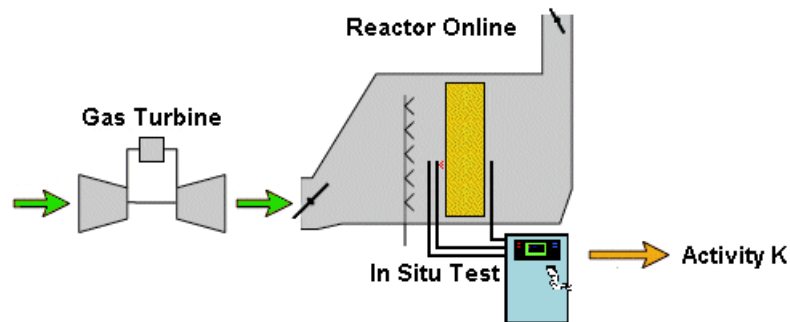


## FERCo's CatalysTrak<sup>®</sup>\*

- *in situ* measurement
- No outage required

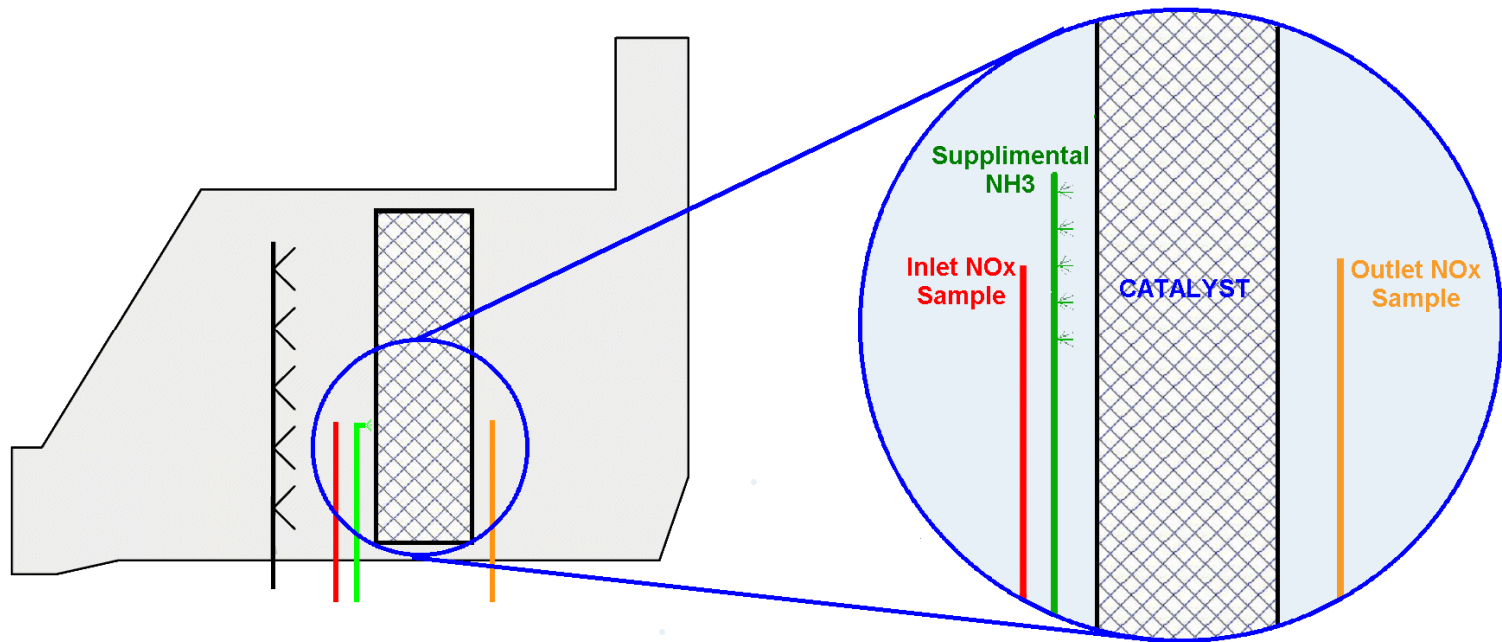
$$K_{\text{In-situ}} = -A_{\text{Vactual}} \ln(1 - \Delta\text{NO}_x)_{\text{full scale}}$$

@NH<sub>3</sub>/NO<sub>x</sub>>1 locally

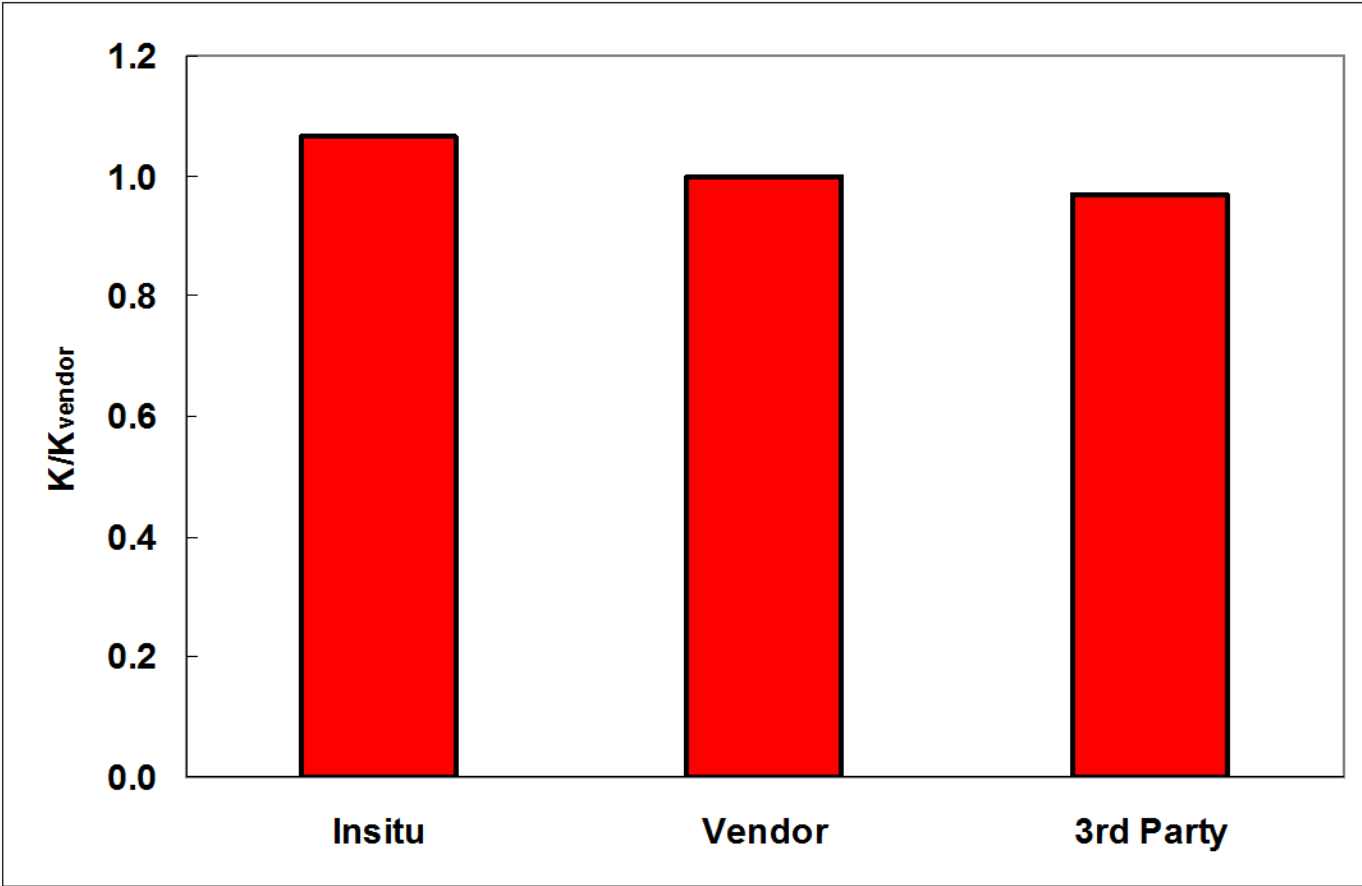


\* Patented Process

# CatalysTrak<sup>®</sup> *In Situ* Test Modules



# In Situ vs Laboratory Activity Measurements



# Summary

- **Troubleshooting**
  - Obtain a curve of NH<sub>3</sub> slip vs Outlet NO<sub>x</sub>
  - Can help distinguish poor NH<sub>3</sub> distribution vs bypass
- **AIG Tuning**
  - Important activity
  - Easy to do with a permanent probe grid installed downstream of the catalyst
- **Flue Gas Bypass and Velocity Profiles**
  - Can be determined with NO<sub>x</sub> measurements
- **CEMs Relative Accuracy**
  - SCR tuning may impact stack NO<sub>x</sub> distribution
- **Catalyst Management/Catalyst Activity**
  - Requires knowledge of Activity vs Time
  - CatalysTrak<sup>®</sup> allows online determination of activity

Questions?

[www.ferco.com](http://www.ferco.com)

